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(54) Title: VANADIUM, RARE EARTH METAL-CONTAINING SPINEL COMPOSITION AND PROCESS OF USING SAME (57) Abstract A composition of matter comprising at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of the first metal, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor amount of at least one vanadium component effective to promote the reduction of first metal sulfate at first metal sulfate reduction conditions. These compositions are useful, e.g., in hydrocarbon conversion processes, to reduce sulfur oxide and/or nitrogen oxide atmospheric emissions.		

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VANADIUM, RARE EARTH
METAL-CONTAINING SPINEL COMPOSITION
AND PROCESS OF USING SAME

This invention relates to improved vanadium, rare earth metal-containing spinel compositions, particularly for use in a manner to effect a reduction in the emission of sulfur oxides and/or nitrogen oxides to the atmosphere. In one specific embodiment, the invention involves compositions and processes for the catalytic cracking of sulfur-containing hydrocarbon feedstocks to effect a reduction in the amount of sulfur oxides and/or nitrogen oxides emitted from the regeneration zone of a hydrocarbon catalytic cracking unit.

Typically, catalytic cracking of hydrocarbons takes place in a reaction zone at hydrocarbon cracking conditions to produce at least one hydrocarbon product and to cause carbonaceous material (coke) to be deposited on the catalyst. Additionally, some sulfur, originally present in the feed hydrocarbons, may also be deposited, e.g., as a component of the coke, on the catalyst.

Sulfur-containing coke deposits tend to deactivate cracking catalyst. Cracking catalyst is advantageously continuously regenerated, by combustion with oxygen-containing gas in a regeneration zone, to low coke levels, typically below about 0.4% by weight, to perform satisfactorily when it is recycled to the reactor. In the regeneration zone, at least a portion of sulfur, along with carbon and hydrogen, which is deposited on the catalyst, is oxidized and leaves in

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the form of sulfur oxides (sulfur dioxide and sulfur trioxide, hereinafter referred to a "SOx") along with substantial amounts of carbon monoxide, carbon dioxide and water. At least a portion of the nitrogen, which may be present in the coke deposits and/or in the oxygen-containing gas, is oxidized at the conditions in the regeneration zone to nitrogen oxides which also leave with the flue gas from the regeneration zone.

Considerable recent research effort has been directed to the reduction of sulfur oxide and nitrogen oxide atmospheric emissions, e.g., from the regeneration zones of hydrocarbon catalytic cracking units. One technique that has been suggested for reducing such sulfur oxide emissions involves circulating one or more metal oxides capable of associating with oxides of sulfur with the cracking catalyst inventory in the regeneration zone. When the particles containing associated oxides of sulfur are circulated to the reducing atmosphere of the cracking zone, the associated sulfur compounds are released as gaseous sulfur-bearing material such as hydrogen sulfide, which is discharged with the products from the cracking zone and is in a form which can be readily handled in a typical facility, e.g., petroleum refinery. The metal reactant is regenerated to an active form, and is capable of further associating with the sulfur oxides when cycled to the regeneration zone.

A metallic component, either incorporated into catalyst particles or present on any of a variety of "inert" supports, is exposed alternately

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to the oxidizing atmosphere of the regeneration zone of an FCCU and the reducing atmosphere of the cracking zone to reduce sulfur oxide emissions from regenerator gases in accordance with the teachings of U.S. Patents Nos. 4,153,534 and 4,153,535 to Vasalos and Vasalos, et al., respectively. In Vasalos, et al., a metallic oxidation promoter, consisting of components of ruthenium, rhodium, palladium, platinum, osmium, iridium, platinum, vanadium, uranium, zirconium, rhenium, silver and mixtures thereof is also present when carbon monoxide emissions are to be reduced. Vasalos, et al., teaches that the more preferred metallic promoter consists of components of ruthenium, rhodium, palladium, osmium, iridium, platinum and rhenium. These patents disclose nineteen different metallic components, including materials as diverse as alkaline earths, sodium, heavy metals and rare earth, as being suitable reactants for reducing emissions of oxides of sulfur. The metallic reactants that are especially preferred are sodium, magnesium, manganese and copper. The carriers for the metallic reactants, preferably have surface areas of at least 50 square meters per gram. Examples of allegedly "inert" supports are silica, alumina and silica-alumina. The Vasalos and Vasalos, et al., patents further disclose that when certain metallic reactants (exemplified by oxides of iron, manganese or cerium) are employed to capture oxides of sulfur, such metallic components can be in the form of a finely divided fluidizable powder.

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A vast number of sorbents have been proposed for desulfurization of non-FCCU flue gases in zones outside the unit in which SO_x is generated. In some such non-FCCU applications, the sorbents are regenerated in environments appreciably richer in hydrogen than the cracking zone of an FCC unit. Fifteen adsorbents are disclosed for flue gas desulfurization in a publication of Lowell, et al., "SELECTION OF METAL OXIDES FOR REMOVING SO_x FROM FLUE GAS," Ind. Eng. Chemical Process Design Development, Vol. 10, Nov. 3, 1971. In U.S. Patent No. 4,001,375 to Longo, cerium on an alumina support is used to absorb SO₂ from non-FCCU flue gas streams or automobile exhaust at temperatures of 572 to 1472 degrees F., preferably 932 to 1100 degrees F.

D. W. Deberry, et al., "RATES OF REACTION OF SO₂ WITH METAL OXIDES," Canadian Journal of Chemical Engineering, 49, 781 (1971) reports that cerium oxide was found to form sulfates more rapidly than most of the other oxides tested. The temperatures used, however, were below 900 degrees F. and thus below those preferred for use in catalyst regenerators in FCC units.

Many commercial zeolitic FCC catalyst contain up to 4% rare earth oxide, the rare earth being used to stabilize the zeolite and provide increased activity. See, for example, U.S. Patent No. 3,930,987 to Grand. The rare earths are most often used as mixtures of La₂O₃, CeO₂, Pr₆O₁₁, Nd₂O₃ and others. Some catalyst is produced by using a lanthanum-rich mixture obtained by removing substantial cerium from the mixture of rare earth.

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It has been found that the mere presence of rare earth in a zeolitic cracking catalyst will not necessarily reduce SOx emissions to an appreciable extent.

In accordance with the teachings of U.S. Patent No. 3,823,092 to Gladrow, certain zeolitic catalyst compositions capable of being regenerated at a rate appreciably faster than prior art rare earth exchanged zeolitic catalyst compositions are produced by treating a previously rare earth exchanged zeolitic catalyst composition with a dilute solution containing cerium cations (or a mixture of rare earths rich in cerium). The final catalysts contain 0.5 to 4% cerium cations which are introduced to previously rare earth exchanged zeolitic catalyst particles prior to final filtering, rinsing and calcining. Cerium is described as an "oxidation promoter".

Thus, considerable amount of study and research effort has been directed to reducing oxide of sulfur emissions from various gaseous streams, including those from the stacks of the regenerators of FCC units. Many metallic compounds have been proposed as materials to pick up oxides of sulfur in FCC units (and other desulfurization applications). Many of the proposed metallic compounds or reactants lose effectiveness when subjected to repeated cycling. Thus, when Group II metal oxides are impregnated on FCC catalysts or various supports, the activity of the Group II metals is rapidly reduced under the influence of the cyclic conditions. Discrete alumina particles, when

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combined with silica-containing catalyst particles and subjected to steam at elevated temperatures, e.g., those present in FCC unit regenerators, are of limited effectiveness in reducing SOx emissions. Incorporation of sufficient chromium on an alumina support to improve SOx sorption results in undesirably increased coke and gas production. The presence of vanadium in the hydrocarbon feedstock to a catalytic cracking unit is known to have a deleterious effect on the cracking operation. For example, this vanadium, which deposits on the catalyst, tends to poison the catalyst, i.e., tends to inhibit the catalyst's ability to promote the desired cracking chemical reactions. This is one reason for the reluctance to even consider the use of vanadium in cracking operations.

U.S. Patents 4,469,589 and 4,472,267, relate to improved materials for reducing SOx emissions comprising spinels, preferably alkaline earth metal, aluminum-containing spinels, which materials may contain one or more other metal components capable of promoting the oxidation of sulfur dioxide to sulfur trioxide at combustion conditions. Such metallic components include components of Group IB metals, Group IIB metals, Group IVB metals, Group VIA metals, Group VIB metals, Group VIIA metals, Group VIII metals, the rare earth metals, vanadium, iron, tin, antimony and mixtures thereof. In specific examples, these patents disclose that magnesium, aluminum-containing spinel is impregnated with such other metal components (e.g., cerium and platinum) using

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conventional techniques. In addition, these patents disclose that in situations where the spinel normally contains aluminum ions, other trivalent metal ions, such as iron, chromium, vanadium, manganese, gallium, boron, cobalt and mixtures thereof, may replace all or a part of the aluminum ions. U.S. Patents 4,471,070; 4,472,532; 4,476,245; 4,492,677; 4,492,678; 4,495,304; 4,495,305 and 4,522,937 also relate to spinel compositions useful to reduce sulfur oxide atmospheric emissions. The specification of each of these patents is incorporated herein by reference. There remains a need for still further improved spinel compositions exhibiting good SOx removal and/or nitrogen oxide reduction properties.

In one general aspect, the present invention involves a composition, hereinafter referred to as "VRS", comprising at least one metal-containing spinel, preferably a major component of such spinel, which includes a first metal and a second metal having a valence higher than the valence of the first metal, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor amount of at least one vanadium component effective to promote the reduction of first metal sulfate at first metal sulfate reduction conditions. In another embodiment, the invention involves a catalyst system comprising, in intimate admixture, a major amount of solid particles capable of promoting hydrocarbon conversion at hydrocarbon

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conversion conditions, and a minor amount of discrete entities having a chemical make-up which is different from the solid particles and which comprise the VRS described above. The present VRS has been found to provide for both outstanding effectiveness in removing sulfur oxides, e.g., from the catalyst regeneration zones of hydrocarbon conversion units, and improved effectiveness in releasing associated sulfur oxide, e.g., in the reaction zones of hydrocarbon conversion units.

A particularly surprising feature of the present invention involves the use of the VRS in hydrocarbon catalytic cracking units. Vanadium is a known catalyst poison in hydrocarbon catalytic cracking units. However, it has been found that the VRS, which contain a vanadium component, provide for outstanding reduction in sulfur oxide and/or nitrogen oxide emissions with no substantial cracking catalyst poisoning.

In a further embodiment, the invention relates to a process for reducing at least one, preferably both, of (1) the sulfur oxide content of a sulfur oxide-containing gas and (2) the nitrogen oxide content of a nitrogen oxide-containing gas which comprises contacting the gas with a composition at conditions to reduce at least one, preferably both, of (1) the sulfur oxide content of the gas and (2) the nitrogen oxide content of the gas. The composition to be used is the VRS first described above.

In yet another embodiment, the present invention relates to an improved hydrocarbon

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conversion, preferably cracking, process for converting a sulfur-containing hydrocarbon feedstock. The process comprises (1) contacting the feedstock with solid particles capable of promoting the conversion of the feedstock at hydrocarbon conversion conditions in at least one reaction zone to produce at least one hydrocarbon product and to cause deactivating sulfur-containing carbonaceous material to be formed on the solid particles; (2) contacting the deposit-containing particles with an oxygen-containing vaporous medium at conditions to combust at least a portion of the carbonaceous deposit material in at least one regeneration zone to thereby regenerate at least a portion of the hydrocarbon conversion catalytic activity of the solid particles and to form a regeneration zone flue gas containing sulfur oxide (e.g., sulfur trioxide) and/or nitrogen oxide; and (3) repeating steps (1) and (2) periodically. In this embodiment, the present improvement comprises using, in intimate admixture with the solid particles, a minor amount of discrete entities having a chemical make-up which is different from the solid particles and which comprise the VRS first described above. Such discrete entities are present in an amount effective to reduce the amount of sulfur oxides and/or nitrogen oxides in the flue gas.

In another embodiment, the discrete entities also include a minor, catalytically effective amount of at least one crystalline material effective to promote hydrocarbon conversion, e.g., cracking, at hydrocarbon conversion conditions.

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The preferred relative amounts of the solid particles and discrete entities are about 80 to about 99 parts and about 1 to about 20 parts by weight, respectively. This catalyst system is especially effective for the catalytic cracking of a hydrocarbon feedstock to lighter, lower boiling products. The present catalyst system also has improved carbon monoxide oxidation catalytic activity stability.

In another embodiment, the VRS has a surface area (by the conventional B.E.T. method) in the range of about $25\text{m}^2/\text{gm.}$ to about $600\text{m}^2/\text{gm.}$, more preferably about $40\text{m}^2/\text{gm.}$ to about $400\text{m}^2/\text{gm.}$, and still more preferably about $50\text{m}^2/\text{gm.}$ to about $300\text{m}^2/\text{gm.}$ These relatively high surface areas have been found to provide for improved reduction in sulfur oxide and/or nitrogen oxide atmospheric emissions.

The improvement of this invention can be used to advantage with the catalyst (solid particles and discrete entities) being disposed in any conventional reactor-regenerator system, in ebullating catalyst bed systems, in systems which involve continuously conveying or circulating catalyst between reaction zone and regeneration zone and the like. Circulating catalyst systems are preferred. Typical of the circulating catalyst bed systems are the conventional moving bed and fluidized bed reactor-regenerator systems. Both of these circulating bed systems are conventionally used in hydrocarbon conversion, e.g., hydrocarbon cracking, operations with the fluidized catalyst bed reactor-regenerator systems being preferred.

Although the presently useful solid particles and discrete entities may be used as a physical admixture of separate particles, in one embodiment, the discrete entities are combined as part of the solid particles. That is, the discrete entities, e.g., comprising calcined microspheres of the VRS, are combined with the solid particles, e.g., during the manufacture of the solid particles, to form combined particles which function as both the presently useful solid particles and discrete entities. In this embodiment, the discrete entities are preferably present as a separate and distinct phase in the combined particles. One preferred method for providing the combined particles is to calcine the discrete entities prior to incorporating the discrete entities into the combined particles.

The form, i.e., particle size, of the present particles, e.g., both solid particles and discrete entities as well as the combined particles, is not critical to the present invention and may vary depending, for example, on the type of reaction-regeneration system employed. Such particles may be formed into any desired shape such as pills, cakes, extrudates, powders, granules, spheres and the like, using conventional methods. Where, for example, the final particles are designed for use as a fixed bed, the particles may preferably be formed into particles having a minimum dimension of at least about 0.01 inch and a maximum dimension of up to about one-half inch or one inch or more. Spherical particles having a diameter of about 0.03 inch to about 0.25 inch, preferably about 0.03 inch

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to about 0.15 inch, are often useful, especially in fixed bed or moving bed operations. With regard to fluidized bed systems, it is preferred that the major amount by weight of the particles have a diameter in the range of about 10 microns to about 250 microns, more preferably about 20 microns to about 150 microns.

The solid particles are capable of promoting the desired hydrocarbon conversion. By "hydrocarbon conversion" is meant a chemical reaction or conversion in which one or more of the feed materials or reactants and/or one or more of the products or conversion products is substantially hydrocarbon in nature, e.g., comprises a major amount of weight of carbon and hydrogen. The solid particles are further characterized as having a composition (i.e., chemical make-up) which is different from the discrete entities. In one preferred embodiment, the solid particles (or the solid particles portion of the combined particles described above) are substantially free of VRS.

The composition of the solid particles useful in the present invention is not critical, provided that such particles are capable of promoting the desired hydrocarbon conversion. Solid particles having widely varying compositions are conventionally used as catalyst in such hydrocarbon conversion processes, the particular composition chosen being dependent, for example, on the type of hydrocarbon chemical conversion desired. Thus, the solid particles suitable for use in the present invention include at least one of the natural or

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synthetic materials which are capable of promoting the desired hydrocarbon chemical conversion. For example, when the desired hydrocarbon conversion involves one or more of hydrocarbon cracking (preferably in the substantial absence of added free molecular hydrogen), disproportionation, isomerization, hydrocracking, reforming, dehydrocyclization, polymerization, alkylation and dealkylation, such suitable materials include acid-treated natural clays, such as montmorillonite, kaolin and bentonite clays; natural or synthetic amorphous materials, such as alumina, silica, silica-alumina, silica-magnesia and silicazirconia composites; and crystalline materials often referred to as zeolites or molecular sieves, such as aluminosilicates, SAPO, TAPO, MeAPO, LZ-210, LZ-10, USY and the like. Certain of these crystalline materials are discussed in U.S. Patents 4,310,440; 4,440,871; 4,500,651; and 4,503,023, the specification of each of which patents is incorporated by reference herein.

In certain instances, e.g., hydrocarbon cracking and disproportionation, the solid particles preferably include such crystalline materials to increase catalytic activity. Methods for preparing such solid particles and the combined solid particles-discrete entities particles are conventional and well known in the art. For example, crystalline aluminosilicate compositions can be made from alkali metal silicates and alkali metal aluminates so that they initially contain significant concentrations of alkali metals. Sodium

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tends to reduce the catalyst activity of the composition for hydrocarbon conversion reactions such as hydrocarbon cracking and disproportionation. Accordingly, most or all of the sodium in the crystalline aluminosilicate is removed or replaced, e.g., with other metal cations such as calcium or aluminum ions or ions of the rare earths, which are associated with the crystalline aluminosilicates. This can be accomplished by contacting the crystalline aluminosilicate with a source of hydrogen ions such as acids, or hydrogen precursors such as ammonium compounds. These procedures are thoroughly described in U.S. Patents 3,140,253 and RE. 27,639.

Compositions of the solid particles which are particularly useful in the present invention are those in which the crystalline materials is incorporated in an amount effective to promote the desired hydrocarbon conversion, e.g., a catalytically effective amount, into a porous matrix which comprises, for example, amorphous material which may or may not be itself capable of promoting such hydrocarbon conversion. Included among such matrix materials are clays and amorphous compositions of alumina, silica, silica-alumina, magnesia, zirconia, mixtures of these and the like. The crystalline material is preferably incorporated into the matrix material in amounts within the range of about 1% to about 75%, more preferably about 2% to about 50%, by weight of the total solid particles. The preparation of crystalline-amorphous matrix catalytic materials is described in the

above-mentioned patents. Catalytically active crystalline materials which are formed during and/or as part of the methods of manufacturing the solid particles, discrete entities and/or as part of the methods of manufacturing the solid particles, discrete entities and/or combined particles are within the scope of the present invention. The solid particles are preferably substantially free of added rare earth metal, e.g., cerium, component disposed on the amorphous matrix material of the catalyst, although such rare earth metal components may be associated with the crystalline materials of the solid particles.

The solid particles useful in the catalytic hydrocarbon cracking embodiment of the present invention may be any conventional catalyst capable of promoting hydrocarbon cracking at the conditions present in the reaction zone, i.e., hydrocarbon cracking conditions. Similarly, the catalytic activity of such solid particles is restored at the conditions present in the regeneration zone. Typical among these conventional catalysts are those which comprise alumina, silica and/or silica-alumina and at least one crystalline aluminosilicate having pore diameters of about 8 angstroms to about 15 angstroms and mixtures thereof. When the solid particles and/or discrete entities to be used in the hydrocarbon cracking embodiment of the present invention contain crystalline aluminosilicate, the crystalline aluminosilicate may include minor amounts of conventional metal promoters such as the rare earth metals, in particular, cerium.

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As indicated above, the present VRS comprise an effective amount, preferably a major amount, of at least one spinel containing a first metal and a second metal, preferably alkaline earth metal-containing spinel, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor amount of at least one vanadium component effective to promote the reduction of first metal, preferably alkaline earth metal sulfate at first metal sulfate reduction conditions. In another aspect, the present VRS include amounts of rare metal component and vanadium component which, are effective to promote the reduction of nitrogen oxides at nitrogen oxide reduction conditions.

The spinel structure is based on a cubic close-packed array of oxide ions. Typically, the crystallographic unit cell of the spinel structure contains 32 oxygen atoms; one-eighth of the tetrahedral holes (of which there are two per anion) are occupied by divalent metal ion, and one-half of the octahedral holes (of which there are two per anion) are occupied by trivalent metal ions.

This typical spinel structure or a modification thereof is adaptable to many other mixed metal oxides of the type $M^{II}M_2^{III}O_4$ (e.g., $FeCr_2O_4$, $ZnAl_2O_4$ and $Co^{II}Co_2^{III}O_4$), by some of the type $M^{IV}M^{II}_2O_4$ (e.g., $TiZn_2O_4$, and $SnCo_2O_4$), and by some of the type $M^I_2M^{VI}O_4$ (e.g., Na_2MoO_4 and Ag_2MoO_4). This structure is often

symbolized as $X[Y_2]O_4$, where square brackets enclose the ions in the octahedral interstices. An important variant is the inverse spinel structure, $Y[XY]O_4$, in which half of the Y ions are in tetrahedral interstices and the X ions are in octahedral ones along with the other half of the Y ions. The inverse spinel structure is intended to be included within the scope of the term "metal-containing spinel" as used herein. The inverse spinel structure occurs often when the X ions have a stronger preference for octahedral coordination than do the Y ions. All $M^{IV}M_2^{II}O_4$ are inverse, e.g., $Zn(ZnTi)O_4$, and many of the $M^{II}M_2^{III}O_4$ ones are also, e.g., $Fe^{III}(Co^{II}Fe^{III})O_4$, $NiAl_2O_4$, $Fe^{III}(Fe^{II}Fe^{III})O_4$ and $Fe(NiFe)O_4$. There are also many compounds with distorted spinel structures in which only a fraction of the X ions are in tetrahedral sites. This occurs when the preference of both X and Y ions are octahedral and tetrahedral sites do not differ markedly.

Further, details on the spinel structure are described in the following references, which are hereby incorporated herein by reference: "Modern Aspects of Inorganic Chemistry" by H. I. Emeleus and A. G. Sharpe (1973), pp. 57-58 and 512- 513; "Structural Inorganic Chemistry", 3rd edition, (1962) by A. F. Wells, pp. 130, 487-490, 503 and 526; and "Advanced Inorganic Chemistry", 3rd edition, by F. A. Cotton and G. Wilkinson (1972), pp. 54-55.

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Metal-containing spinels include the following: MnAl_2O_4 , FeAl_2O_4 , CoAl_2O_4 , NiAl_2O_4 , ZnAl_2O_4 , MgTiMgO_4 , FeMgFeO_4 , FeTiFeO_4 , ZnSnZnO_4 , GaMgGaO_4 , InMgInO_4 , BeLi_2F_4 , MoLi_2O_4 , SnMg_2O_4 , MgAl_2O_4 , CuAl_2O_4 , $(\text{LiAl}_5\text{O}_8)$, $\text{ZnK}_2(\text{CN})_4$, $\text{CdK}_2(\text{CN})_4$, $\text{HgK}_2(\text{CN})_4$, ZnTi_2O_4 , FeV_2O_4 , MgCr_2O_4 , MnCr_2O_4 , FeCr_2O_4 , CoCr_2O_4 , NiCr_2O_4 , ZnCr_2O_4 , CdCr_2O_4 , MnCr_2S_4 , ZnCr_2S_4 , CdCr_2S_4 , TiMn_2O_4 , MnFe_2O_4 , FeFe_2O_4 , NiFe_2O_4 , CuFe_2O_4 , CdFe_2O_4 , MgCo_2O_4 , TiCo_2O_4 , CoCo_2O_4 , ZnCo_2O_4 , SnCo_2O_4 , CoCo_2S_4 , CuCo_2S_4 , GeNi_2O_4 , NiNi_2S_4 , ZnGa_2O_4 , WAg_2O_4 , and ZnSn_2O_4 .

The presently useful metal-containing spinels include a first metal and a second metal having a valence (oxidation state) higher than the valence of the first metal. The first and second metals may be the same metal or different metals. In other words, the same metal may exist in a given spinel in two or more different oxidation states. As indicated above, the atomic ratio of the first metal to the second metal in any given spinel need not be consistent with the classical stoichiometric formula for such spinel. In one embodiment, the atomic ratio of the first metal to the second metal in the metal-containing spinel useful in the present invention is at least about 0.17 and preferably at least about 0.25. If the first metal is a mono-valent metal, the atomic ratio of the first

metal to the second metal is preferably at least about 0.34, more preferably at least about 0.5.

The preferred metal-containing spinels for use in the present invention are alkaline earth metal spinels, in particular magnesium (first metal) and aluminum (second metal)-containing spinel. Other alkaline earth metal ions, such as calcium, strontium, barium and mixtures thereof, may replace all or a part of the magnesium ions. Similarly, other metal ions, such as iron, chromium, vanadium, manganese, gallium, boron, cobalt, Group IB metals, Group IV metals, Group VA metals, the platinum group metals, the rare earth metals, Te, Nb, Ta, Sc, Zn, Y, Mo, W, Tl, Re, U, Th and mixtures thereof, may replace all or a part of the aluminum ions, preferably only a part of the aluminum ions. When the spinel includes a divalent metal (e.g., magnesium) and a trivalent metal (e.g., aluminum), it is preferred that the atomic ratio of divalent to trivalent metals in the spinel be in the range of about 0.17 to about 2.5, more preferably about 0.25 to about 2.0, and still more preferably about 0.35 to about 1.5.

The metal-containing spinels useful in the present invention may be derived from conventional and well known sources. For example, these spinels may be naturally occurring or may be synthesized using techniques well known in the art. Thus, a detailed description of such techniques is not included herein. A particularly useful process for preparing the VRS is presented in U.S. patent application Serial No. (Attorney Docket

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No. 15367), the specification of which is incorporated by reference herein.

Substantially non-interfering proportions of other well known refractory material, e.g., inorganic oxides such as silica, zirconia, thoria and the like may be included in the present VRS. By substantially "non-interfering" is meant amounts of the material which do not have a substantial deleterious effect on the intended functionality of the present VRS, catalyst system, or hydrocarbon conversion process, as the case might be. The inclusion of materials such as silica, silica-alumina, zirconia, thoria and the like into the present VRS may act to improve one or more of the functions of the VRS. Free magnesia and/or alumina (i.e., apart from the alkaline earth metal containing spinel) also may be included in the present VRS, e.g., using conventional techniques. For example, in one embodiment the VRS preferably includes about 0.1% to about 30% by weight of free magnesia (calculated as MgO). Such free magnesia may act to improve the effectiveness of the VRS to reduce sulfur oxide and/or nitrogen oxide atmospheric emissions.

The rare earth metal component and the vanadium component may be associated with the spinel using impregnation, ion-exchange and the like, well known in the art. These metal components may be associated with the spinel together or in any sequence. Impregnation may be carried out by contacting the spinel with a solution, preferably an aqueous solution, of rare earth and vanadium salts.

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Water-soluble sources of rare earth and vanadium include the nitrate, acetate and chloride.

Preferably, the present VRS include about 0.1% to about 20%, more preferably about 0.1% to about 15%, and still more preferably about 2% to about 15%, by weight of rare earth metal, calculated as elemental metal; and about 0.05% to about 7%, more preferably about 0.1% to about 5%, and still more preferably about 0.2% to about 2% by weight of vanadium, calculated as elemental metal.

It may not be necessary to wash the spinel after certain soluble rare earth and vanadium salts (such as nitrate or acetate) are added. After impregnation with rare earth and vanadium salts, the spinel can be dried and calcined to decompose the salts, forming an oxide in the case of nitrate or acetate. Alternately the spinel, e.g., in the form of discrete particles, can be charged to a hydrocarbon conversion, e.g., cracking, unit with the rare earth and vanadium in salt form. In this case, the rare earth and vanadium salts with thermally decomposable anions can decompose to the oxides in the unit.

The present discrete entities may further comprise a minor amount of at least one crystalline material capable of promoting the desired hydrocarbon conversion. Typical crystalline materials have been described above. Such crystalline materials may comprise about 1% to about 30%, for example about 1% to about 10%, by weight of the discrete entities. The presence of such crystalline materials in the present discrete

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entities acts to increase the overall catalytic activity of the solid particles-discrete entities mixture for promoting the desired hydrocarbon conversion.

Preferably, these metal components are substantially uniformly disposed in or on the VRS.

Included among the rare earth metals useful in the present invention are the Lanthanum or Lanthanide Series (of the Periodic Chart of Elements) metals and mixtures thereof. The preferred rare earth metals are selected from the group consisting of cerium, praseodymium, lanthanum and mixtures thereof, with cerium being more preferred.

As noted above, the presently useful solid particles and discrete entities can be employed in a mass of combined particles which function as both the solid particles, e.g., promotes hydrocarbon conversion, and the discrete entities. Such combined particles may be produced in any suitable manner, certain of which methods are conventional and known in the art.

Although this invention is useful in many hydrocarbon conversions, the present catalyst, i.e., mixture comprising solid particles and discrete entities, and hydrocarbon conversion process find particular applicability in systems for the catalytic cracking of hydrocarbons where oxidative and regeneration of catalyst is employed. Such catalytic hydrocarbon cracking often involves converting, i.e., cracking, heavier or higher boiling components, to gasoline and other lower

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boiling components, such as hexane, hexene, pentane, pentene, butane, butylene, propane, propylene, ethane, ethylene, methane and mixtures thereof. Often, the substantially hydrocarbon feedstock comprises a gas oil fraction, e.g., derived from petroleum, shale oil, tar sand oil, coal and the like. Such feedstock may comprise a mixture of straight run, e.g., virgin, gas oil. Such gas oil fractions often boil primarily in the range of about 400 degrees F. to about 1000 degrees F. Other substantially hydrocarbon feedstocks, e.g., naphtha, high boiling or heavy fractions of petroleum, petroleum residuum, shale oil, tar sand oil, coal and the like, may be cracked using the catalyst and method of the present invention. Such substantially hydrocarbon feedstock often contains minor amounts of other elements, e.g., sulfur, nitrogen, oxygen and the like. In one aspect, the present invention involves converting a hydrocarbon feedstock containing sulfur and/or sulfur chemically combined with the molecules of hydrocarbon feedstock. The present invention is particularly useful when the amount of sulfur in such hydrocarbon feedstock is in the range of about 0.01% to about 5%, preferably about 0.1% to about 3%, by weight of the total feedstock.

Hydrocarbon cracking conditions are well known and often include temperatures in the range of about 850 degrees F. to about 1100 degrees F., preferably about 900 degrees F. to about 1050 degrees F. Other reaction conditions usually include pressures of up to about 100 psia.; catalyst

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to oil ratios of about 1 to 2 to about 25 to 1, preferably about 3 to 1 to about 15 to 1; and weight hourly space velocities (WHSV) of about 3 to about 60. These hydrocarbon cracking conditions may be varied depending, for example, on the feedstock and solid particles or combined particles being used, the reactor-regenerator system, e.g., fluid or moving bed catalytic cracking system, being employed, and the product or products wanted.

In addition, the catalytic hydrocarbon cracking system includes a regeneration zone for restoring the catalytic activity of the solid particles or combined particles of catalyst previously used to promote hydrocarbon cracking. Carbonaceous, in particular sulfur-containing carbonaceous, deposit-containing catalyst particles from the reaction zone are contacted with free oxygen-containing gas in the regeneration zone at conditions to restore or maintain the activity of the catalyst by removing, i.e., combusting, at least a portion of the carbonaceous material from the catalyst particles. When the carbonaceous deposit material contains sulfur, at least one sulfur-containing combustion product is produced in the regeneration zone and may leave the zone with the regenerator flue gas. The conditions at which such free oxygen-containing gas contacting takes place may vary, for example, over conventional ranges. The temperature in the catalyst regeneration zone of a hydrocarbon cracking system are often in the range of about 900 degrees F. to about 1500 degrees F., preferably about 1100 degrees

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F. to about 1350 degrees F. and more preferably about 1100 degrees F. to about 1300 degrees F. Other conditions within such regeneration zone may include, for example, pressures up to about 100 psia., and average catalyst contact times within the range of about 3 minute to about 75 minutes. Sufficient oxygen is preferably present in the regeneration zone to completely combust the carbon and hydrogen of the carbonaceous deposit material, for example, to carbon dioxide and water. The amount of carbonaceous material deposited on the catalyst in the reaction zone is preferably in the range of about 0.005% to about 15%, more preferably about 0.1% to about 5% by weight of the catalyst. The amount of sulfur, if any, contained in the carbonaceous deposit material depends, for example, on the amount of sulfur in the hydrocarbon feedstock. This deposit material may contain about 0.01% to about 10% or more by weight of sulfur. At least a portion of the regenerated catalyst is often returned to the hydrocarbon cracking reaction zone.

One embodiment of the present invention involves contacting sulfur oxide and/or nitrogen oxide-containing gases, e.g., combustion products, with the present VRS. Reduced concentrations of sulfur oxide and/or nitrogen oxide, e.g., reduced emissions of sulfur oxide and/or nitrogen oxide from the combustion zones, are achieved as a result of this contacting.

Typical combustion zones include, for example, fluid bed coal burning steam boilers and fluid sand bed waste combustors. In the coal fired

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boiler application, the present VRS may be added, either separately or with the sulfur-containing coal, to the combustion zone, e.g., boiler, where combustion takes place. The present VRS then leave the combustion zone with the coal ash and can be separated from the ash, e.g., by screening, density separation, or other well known solids separation techniques. In one embodiment, the sulfur oxide-containing gases are contacted with the present VRS at conditions to reduce the sulfur oxide content of the gases in one or more zones, e.g., separate from the combustion zone. In any event, the flue gases leaving the combustion zone/contacting zone system have reduced amounts of sulfur oxide and/or nitrogen oxide, e.g., relative to processing in the absence of the present VRS. The VRS from the combustion zone or contacting zone can be subjected to a reducing environment, e.g., contacted with hydrogen, hydrocarbon and the like reducing media, at conditions such that at least a portion of the sulfur associated with the VRS is disassociated, e.g., in the form of hydrogen sulfide and is removed for further processing, e.g., sulfur recovery. The VRS, after sulfur removal may be recycled to the combustion zone or contacting zone.

Conditions within such contacting zones may be those typically used in contact zones employing conventional sulfur oxide or nitrogen oxide removal agents. The amount of the present VRS used to contact a sulfur oxide-containing and/or nitrogen oxide-containing gas is sufficient to reduce the sulfur oxide and/or nitrogen oxide content of the

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gas, preferably, by at least about 50% and more preferably by at least 80%. Reducing conditions are such that at least a portion, preferably at least about 50% and more preferably at least about 80% of the sulfur associated with the VRS is removed. For example, reducing conditions may include temperatures in the range of about 900 degrees F., hydrogen hydro 14 to abcarbon and the like, to associated sulfur mole ratio in the range of about 1 to about 10.

The following examples are provided to better illustrate the invention, without limitation, by presenting several specific embodiments of the compositions and processes of the invention.

EXAMPLES 1 TO 14

A series of magnesium, aluminum-containing spinel compositions were prepared as follows.

Magnesium, aluminum-containing spinel particles were prepared using conventional co-precipitation/calcining techniques. The resulting spinel had a surface area of more than $100\text{m}^2/\text{gm.}$; and an atomic ratio of magnesium to aluminum of 0.77. The average particle size of the spinel particles was in the range of about 65 microns.

Fourteen portions of these spinel particles were subjected to conventional impregnation/calcining techniques using aqueous solutions of various metal salts to prepare the following fourteen compositions*:

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<u>Composition</u>	<u>Wt. % of Metal (as Elemental Metal) Included with the Spinel Particles</u>
Example 1	5% Cerium
Example 2	10% Cerium
Example 3	20% Cerium
Example 4	10% Praseodymium
Example 5	10% Lanthanum
Example 6	10% Iron
Example 7	10% Manganese
Example 8	10% Cobalt
Example 9	5% Vanadium
Example 10	2% Vanadium/10% Cerium**
Example 11	10% Tin
Example 12	5% Tin/5% Cerium
Example 13	1% Iron/10% Cerium
Example 14	5% Iron/5% Tin

* When two metals are included with the spinel particles, the spinel particles were impregnated with both metals simultaneously.

** $(\text{NH}_4)\text{VO}_3$ and $\text{Ce}(\text{NO}_3)_3$ salts employed in preparation.

The impregnation/calcining of the various portions of the spinel particles did not substantially change the surface area of the spinel or the size of the particles.

Examples 15-28

A quantity of solid particles of a commercially available, crystalline aluminosilicate hydrocarbon cracking catalyst, having the same approximate particle size distribution as the spinel-containing particles from Examples 1 to 14, was combined with each of the final products of Examples 1 to 14 so that mixtures of 1.75 parts by weight of the spinel-containing particles (discrete entities) and 98.25 parts by weight of the solid

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particles resulted. The catalytic activity of the solid particles was equilibrated by use (prior to combining with the discrete entities) in commercial fluid bed catalytic cracking service.

Each blend was tested to determine its ability to continue to remove sulfur oxides over a period of time. This test procedure was as follows: Step 1 involved an initial determination of the ability of the blend to remove sulfur oxides from regenerator flue gases. Step one was carried out in a fluid bed catalytic cracking pilot plant known to provide results which are correlatable to results obtained in commercial sized systems.

The feedstock and conditions for step 1 were as follows:

Feedstock - mid-continent gas oil

containing about 2% by weight sulfur

Reactor temperature - 1000 degrees F.

Regenerator temperature - 1280 degrees F.

Stripper temperature - 930 degrees F.

Pressure - 15 psia.

Approximate catalyst regeneration time -
30 minutes

Catalyst to oil weight ratio - 6

Weight hourly space velocity - 10

Steam as inerts in reactor, 3 mole %.

Step 2 of the test procedure involved continuous and accelerated aging in a fluidized-bed reactor to simulate the type of aging which occurs in commercial fluid-bed catalytic cracking service. The feedstock and conditions utilized in step 2 were as follows:

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Feedstock - mid-continent gas oil
containing 2% by weight sulfur.
Reactor temperature - 1150 degrees F.
Reactor pressure - 15 psig.
Reaction catalyst/oil weight ratio - 15
Weight hourly space velocity - 0.8
Regenerator temperature - 1350 degrees F.
Regenerator pressure - 15 psig.
Catalyst regenerator residence time -
30 minutes
Regenerator combustion air flow ratio -
20 lbs. air/lb. coke
Cycles per day - 11

Step 3 of the test procedure involved periodically repeating step 1 to determine how much of the blend's activity to remove sulfur oxide had been lost during the aging of step 2.

The amount of total sulfur oxides emitted with the flue gases from the regeneration using the blend was used as the basis for determining the blend's ability (or activity) to remove such sulfur oxides.

Results of testing these blends were as follows:

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RELATIVE ACTIVITY TO
REMOVE SULFUR OXIDES

Example 1 Virgin	52
Example 1 Aged 2 days	--
Example 2 Virgin	83
Example 2 Aged 2 days	32
Example 3 Virgin	83
Example 3 Aged 2 days	42
Example 4 Virgin	32
Example 4 Aged 2 days	--
Example 5 Virgin	40
Example 5 Aged 2 days	31
Example 6 Virgin	31
Example 6 Aged 2 days	--
Example 7 Virgin	36
Example 7 Aged 2 days	--
Example 8 Virgin	6
Example 8 Aged 2 days	--
Example 9 Virgin	81
Example 9 Aged 2 days	27
Example 10 Virgin	96
Example 10 Aged 2 days	78
Example 11 Virgin	less than 25
Example 11 Aged 2 days	--
Example 12 Virgin	56
Example 12 Aged 2 days	--
Example 13 Virgin	88
Example 13 Aged 2 days	38
Example 14 Virgin	47
Example 14 Aged 2 days	--

These data indicate clearly that a composition according to the present invention,

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i.e., Composition 10, has both outstanding initial sulfur oxide removal activity and outstanding sulfur oxide removal activity stability, i.e., the ability to maintain sulfur oxide removal activity over a period of time.

Samples of virgin and aged Composition 10 were taken from a point between the reaction zone and the regeneration zone of the above-noted catalytic cracking pilot plant and were analyzed for sulfur content. It was found that the sulfur contents of these samples was significantly lower than those of other materials, such as Compositions 1, 2 and 3. Thus, it appears that the spinel-containing discrete entities of Composition 10 have reduced sulfur contents coming out of the reaction zone. This, in turn, means that Composition 10 has an increased kinetic driving force for sulfur oxide removal in the regeneration zone. In any event, the present vanadium, rare earth-containing spinel compositions do provide substantial sulfur oxide removal.

Example 29

This example illustrates the experimental trial of an embodiment of the present invention in a commercial-sized catalytic cracking unit.

Magnesium, aluminum-containing spinel particles were prepared using a co-precipitation/calcining technique. The resulting spinel had a surface area of more than $100\text{m}^2/\text{gm.}$; and an atomic ratio of magnesium to aluminum of 0.91. The average particle size of these spinel particles was in the range of about 65 microns.

This spinel material was subjected to a conventional impregnation/calcining technique using an aqueous solution containing cerium ($\text{Ce}(\text{NO}_3)_3$) and vanadium ($(\text{NH}_4)\text{VO}_3$) salts. The final spinel-containing particles included 10% by weight of cerium and 1% by weight of vanadium, calculated as the elemental metals.

These final spinel-containing particles were tested in a commercial sized fluid-bed catalytic cracking (FCC) unit having a catalytic inventory of about 170 tons and used to crack a gas oil feedstock containing about 0.4% by weight of sulfur.

Briefly, such FCC units involve a riser/vessel and a second vessel in at least limited fluid communication with each other. The riser/vessel serves as a reaction zone. Hydrocarbon feedstock and catalyst particles are fed to the riser/vessel reaction zone at hydrocarbon cracking conditions. At least a portion of the hydrocarbon cracking occurs in this reaction zone, where the catalyst and hydrocarbon form one or more fluid phases.

Catalyst and hydrocarbon are continuously drawn from the reaction zone. The hydrocarbon is sent for further processing, distillation and the like. Catalyst, stripped of hydrocarbon, flows to the second vessel, a catalyst regeneration zone, where it is combined with air at proper conditions to combust at least a portion of the carbonaceous deposits from the catalyst formed during the hydrocarbon cracking reaction. The catalyst and

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vapors in the regeneration zone form a fluid phase or bed. Catalyst is continuously removed from the regeneration zone and is combined with the hydrocarbon feedstock prior to being fed to the reaction zone.

During the test period, the weight ratio of catalyst particles (including the final spinel-containing particles noted above) to total (fresh plus recycle) hydrocarbon feed entering the reaction zone was about 6 to 1. Other typical conditions within the reaction zone include:

Temperature, degrees F. 965

WHSV about 40

Such conditions resulted in about 70% by volume conversion of the gas oil feedstock to products boiling at 400 degrees F. and below.

The catalyst particles from the reaction zone included about 0.8% by weight of carbonaceous deposit material which was at least partially combusted in the regeneration zone. This carbonaceous material also included a minor amount of sulfur which forms SO_2 at the combustion conditions formed in the regeneration zone. Air, in an amount so that amount of oxygen in the regeneration zone was about 1.15 times the amount theoretically required to completely combust this deposit material, was heated to the desired temperature before being admitted to the regeneration zone.

Conditions within the regeneration zone included:

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Temperature, degrees F.	1310
Average catalyst	
Residence Time, min.	10
Average Flue Gas oxygen content	4.5

During the test period about 300 pounds per day of the final spinel-containing particles were added. Daily additions of about 5 tons of catalyst particles were made to compensate the catalyst inventory for catalyst attrition losses and to maintain the desired level of catalytic activity. The maximum concentration of the spinel-containing particles in the catalyst inventory over the fifteen day test period was about 0.45% by weight. Toward the end of the test period sulfur oxide emissions from this FCC unit were being reduced by more than 80% relative to the sulfur oxide emissions from this FCC unit prior to the addition of the spinel-containing particles.

The effectiveness of the present spinel-containing particles in reducing sulfur oxide emissions is substantially greater than with certain other spinel-containing particles. For example, in order to achieve 80% reduction in sulfur oxide emissions with spinel-containing particles including 10% by weight of cerium, calculated as elemental cerium, and substantially no vanadium, a concentration level in the FCC unit catalyst inventory of 0.75% by weight is required. The present compositions which include both rare earth metal and vanadium are clearly superior.

Examples 30-34

These Examples illustrate certain preferred embodiments of the present invention

Magnesium, aluminum-containing spinel particles were prepared using a co-precipitation/calcining technique. The resulting spinel had a surface area of more than $100\text{m}^2/\text{gm}$. and an atomic ratio of magnesium to aluminum of about 0.5. The average particle size of the spinel particles was in the range of about 65 microns.

Separate portions of these spinel particles were subjected to a conventional impregnation/calcining technique using aqueous solutions containing various amounts of cerium and vanadium salts. Each portion of the final spinel-containing particles included the following amount of cerium and vanadium, calculated as elemental metal:

<u>COMPOSITION</u>	<u>% Cerium</u>	<u>% Vanadium</u>
Example 30	10	2
Example 31	10	2
Example 32	10	0.6
Example 33	10	3
Example 34	10	1.2

Each of these spinel-containing compositions was combined with a quantity of commercially available hydrocarbon cracking catalyst particles described above in Examples 15 to 28 so that mixtures of 1.75 parts by weight of the spinel-containing composition and 98.25 parts by weight of the cracking catalyst particles results.

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Each of these blends was tested to determine its ability to reduce the nitrogen oxide (NOx) content of the flue gases from a cracking catalyst regeneration zone. Thus each of these blends was subjected to twenty two reaction/regeneration cycles using step (2) of the test procedure set forth above in Examples 15 to 28. After this aging, the blend was tested in accordance with step (1) of the above-noted test procedure and the nitrogen oxide content of the regeneration zone flue gases was measured. Results of these tests were as follows:

NITROGEN OXIDE CONCENTRATION	
	vppm (1) (2)
	With Agent
10% Ce / 2% V	200-400
10% Ce / 2% V	100-200
10% Ce / 0.6% V	100-300
10% Ce / 3% V	300-500
10% Ce / 1.2% V	50-100

- (1) The amount of nitrogen oxide present in the flue gases with no spinel-containing particles added was estimated at 250-400vppm.
- (2) The amount of nitrogen oxide present in the flue gases with a comparable amount of spinel-containing particles including (1) only 10% by weight of cerium; and (2) only 5% by weight of vanadium was (1) 400-500 vppm., and (2) 350-400 vppm., respectfully.

These results indicate that spinel-containing compositions which include rare earth metal component and vanadium component do

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provide for reduction in nitrogen oxide emissions from combustion zone flue gases. Such compositions which include about 0.2% to about 2%, more particularly about 0.5% to about 1.5%, by weight of vanadium component (calculated as elemental vanadium) provide outstanding reductions in such nitrogen oxide emissions.

While this invention has been described with respect to various specific examples and embodiments, it is to be understood that the invention is not limited thereto and that it can be variously practiced within the scope of the following claims.

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CLAIMS

1. A composition of matter comprising at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first metal, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor amount of at least one vanadium component effective to promote the reduction of first metal sulfate at first metal sulfate reduction conditions.
2. The composition of claim 1 wherein said spinel has a surface area in the range of about $25\text{m}^2/\text{gm.}$ to about $600\text{m}^2/\text{gm.}$
3. The composition of claim 2 wherein said composition comprises a major amount by weight of said spinel.
4. The composition of claim 1 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.05% to about 7% by weight calculated as elemental vanadium metal.
5. The composition of claim 1 wherein at least one of said rare earth metal component and said vanadium component is incorporated in said composition by impregnation.

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6. The composition of claim 1 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

7. The composition of claim 1 wherein said rare earth metal component and said vanadium component are present in amounts effective to promote the reduction of nitrogen oxides at nitrogen oxide reduction conditions.

8. The composition of claim 8 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.1% to about by weight, calculated as elemental vanadium metal.

9. The composition of claim 7 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 15% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.2% to about 2% by weight, calculated as elemental vanadium metal.

10. The composition of claim 4 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

11. The composition of claim 9 wherein said spinel comprises alkaline earth metal-containing

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spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

12. The composition of claim 6 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

13. The composition of claim 10 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

14. The composition of claim 11 wherein said spinel includes magnesium and aluminum, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

15. The composition of claim 12 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

16. The composition of claim 13 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

17. The composition of claim 14 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

18. The composition of claim 1 wherein said rare earth metal component is a cerium component.

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19. The composition of claim 4 wherein said rare earth metal component is a cerium component.

20. The composition of claim 9 wherein said rare earth metal component is a cerium component.

21. A process for reducing at least one of (1) the sulfur oxide content of a sulfur oxide-containing gas and (2) the nitrogen oxide content of a nitrogen oxide-containing gas which comprises contacting said gas with a material at conditions to reduce at least one of (1) the sulfur oxide content of said gas and (2) the nitrogen oxide content of said gas, said material comprising at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first spinel, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor amount of at least one vanadium component effective to promote the reduction of first metal sulfate at first metal sulfate reduction conditions.

22. The process of claim 21 wherein said spinel has a surface area in the range of about $25\text{m}^2/\text{gm.}$ to about $600\text{m}^2/\text{gm.}$

23. The process of claim 22 wherein said composition comprises a major amount by weight of said spinel.

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24. The process of claim 21 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.05% to about 7% by weight, calculated as elemental vanadium metal.

25. The process of claim 21 wherein at least one of said rare earth metal component and said vanadium component is incorporated in said material by impregnation.

26. The process of claim 21 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

27. The process of claim 21 wherein said rare earth metal component and said vanadium component are present in amounts effective to promote reduction of nitrogen oxides at nitrogen oxide reduction conditions.

28. The process of claim 27 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 15% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.1% to about 5% by weight, calculated as elemental vanadium metal.

29. The process of claim 28 wherein said rare earth metal component is present in an amount

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in the range of about 0.1% to about 15% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.2% to about 2% by weight, calculated as elemental vanadium.

30. The process of claim 24 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

31. The process of claim 29 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

32. The process of claim 26 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

33. The process of claim 30 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

34. The process of claim 31 wherein said spinel includes magnesium as said first metals and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

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35. The process of claim 32 wherein said material further comprises about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

36. The process of claim 33 wherein said material further comprises about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

37. The process of claim 34 wherein said material further comprises about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

38. The process of claim 21 wherein said rare earth metal component is a cerium component.

39. The process of claim 24 wherein said rare earth metal component is a cerium component.

40. The process of claim 29 wherein said rare earth metal component is a cerium component.

41. A composition of matter comprising, in intimate admixture, a major amount of solid particles capable of promoting hydrocarbon conversion at hydrocarbon conversion conditions, and a minor amount of discrete entities having a chemical make-up different from said solid particles and comprising at least one metal-containing spinel which includes a first metal and a second metal having a valence higher than the valence of said first metal, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor

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amount of at least one vanadium component effective to promote the reduction of first metal sulfate at first metal sulfate reduction conditions.

42. The composition of claim 41 wherein said hydrocarbon conversion comprises hydrocarbon cracking in the substantial absence of added molecular hydrogen, at least one of said solid particles and discrete entities includes crystalline aluminosilicate effective to promote said hydrocarbon cracking and a major amount by weight of said solid particles have diameters in the range of about 10 microns to about 250 microns.

43. The composition of claim 41 wherein said discrete entities contain a major amount by weight of said spinel and said spinel has a surface area in the range of about $25\text{m}^2/\text{gm.}$ to about $600\text{m}^2/\text{gm.}$

44. The composition of claim 41 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.05% to about 7% by weight, calculated as elemental vanadium metal.

45. The composition of claim 41 wherein at least one of said rare earth metal component and said vanadium component is incorporated in said discrete entities by impregnation.

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46. The composition of claim 41 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

47. The composition of claim 41 wherein said rare earth metal component and said vanadium component are present in amounts effective to promote the reduction of nitrogen oxides at nitrogen oxide reduction conditions.

48. The composition of claim 47 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight of said discrete entities, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.1% to about 5% by weight of said discrete entities, calculated as elemental vanadium metal.

49. The composition of claim 47 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight of said discrete entities, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.2% to about 2% by weight of said discrete entities, calculated as elemental vanadium.

50. The composition of claim 44 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to second metal is at least about 0.17.

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51. The composition of claim 49 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

52. The composition of claim 46 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

53. The composition of claim 50 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

54. The composition of claim 51 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

55. The composition of claim 52 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

56. The composition of claim 53 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

57. The composition of claim 54 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

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58. The composition of claim 41 wherein said rare earth metal component is a cerium component.

59. The composition of claim 44 wherein said rare earth metal component is a cerium component.

60. The composition of claim 49 wherein said rare earth metal component is a cerium component.

61. In a hydrocarbon conversion process for converting a sulfur-containing hydrocarbon feedstock which comprises (1) contacting said feedstock with solid particles capable of promoting the conversion of said feedstock at hydrocarbon conversion conditions in at least one reaction zone to produce at least one hydrocarbon product and to cause deactivating sulfur-containing carbonaceous material to be formed on said solid particles thereby forming deposit-containing particles; (2) contacting said deposit-containing particles with an oxygen-containing vaporous medium at conditions to combust at least a portion of said carbonaceous deposit material in at least one regeneration zone to thereby regenerate at least a portion of the hydrocarbon conversion catalytic activity of said solid particles and to form a regeneration zone flue gas containing sulfur oxide and/or nitrogen oxide; and (3) repeating steps (1) and (2) periodically, the improvement which comprises, using, in intimate admixture with said solid particles, a minor amount

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of discrete entities having a chemical make-up different from said solid particles and comprising at least one metal-containing spinel including a first metal and a second metal having a valence higher than the valence of said first metal, a minor amount of at least one rare earth metal component effective to promote the oxidation of sulfur dioxide to sulfur trioxide at sulfur dioxide oxidation conditions, and a minor amount of at least one vanadium component effective to promote the reduction of first metal sulfate at first metal sulfate reduction conditions, said discrete entities being present in an amount sufficient to reduce the amount of sulfur oxides and/or nitrogen oxide in said flue gas.

62. The process of claim 61 wherein said hydrocarbon conversion comprises hydrocarbon cracking in the substantial absence of added molecular hydrogen, at least one of said solid particles and discrete entities include a crystalline aluminosilicate effective to promote said hydrocarbon cracking and a major amount, by weight of said solid particles have diameters in the range of about 10 microns to about 250 microns.

63. The process of claim 61 wherein said discrete entities contain a major amount by weight of said spinel and said spinel has a surface area in the range of about $25\text{m}^2/\text{gm.}$ to about $600\text{m}^2/\text{gm.}$

64. The process of claim 61 wherein said rare earth metal component is present in an amount

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in the range of about 0.1% to about 20% by weight of said discrete entities, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.05% to about 7% by weight of said discrete entities, calculated as elemental vanadium metal.

65. The process of claim 61 wherein at least one of said rare earth metal component and said vanadium component is incorporated in said composition by impregnation.

66. The process of claim 61 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

67. The process of claim 61 wherein said rare earth metal component and said vanadium component are present in amounts effective to promote the reduction of nitrogen oxides at nitrogen oxide reduction conditions, and said discrete entities discrete entities are present in an amount sufficient to reduce the amount of nitrogen oxides in said flue gas.

68. The process of claim 61 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight of said discrete entities, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.1% to about 5% by weight of said discrete entities, calculated as elemental vanadium metal.

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69. The process of claim 67 wherein said rare earth metal component is present in an amount in the range of about 0.1% to about 20% by weight of said discrete entities, calculated as elemental rare earth metal, and said vanadium component is present in an amount in the range of about 0.2% to about 2% by weight of said discrete entities, calculated as elemental vanadium.

70. The process of claim 64 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

71. The process of claim 69 wherein said spinel comprises alkaline earth metal-containing spinel and the atomic ratio of said first metal to said second metal is at least about 0.17.

72. The process of claim 66 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

73. The process of claim 70 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio of magnesium to aluminum in said spinel is at least about 0.25.

74. The process of claim 71 wherein said spinel includes magnesium as said first metal and aluminum as said second metal, and the atomic ratio

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of magnesium to aluminum in said spinel is at least about 0.25.

75. The process of claim 72 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

76. The process of claim 73 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.

77. The process of claim 74 further comprising about 0.1% to about 30% by weight of free magnesia, calculated as MgO.


78. The process of claim 61 wherein said rare earth metal component is a cerium component.

79. The process of claim 64 wherein said rare earth metal component is a cerium component.

80. The process of claim 69 wherein said rare earth metal component is a cerium component.

INTERNATIONAL SEARCH REPORT

International Application No. PCT/US 87/00749

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) *		
According to International Patent Classification (IPC) or to both National Classification and IPC		
IPC ⁴ : B 01 J 23/00; C 01 F 7/16; C 10 G 11/04		
II. FIELDS SEARCHED		
Minimum Documentation Searched ⁷		
Classification System	Classification Symbols	
IPC ⁴	B 01 J; C 10 G; C 01 F	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched *		
III. DOCUMENTS CONSIDERED TO BE RELEVANT *		
Category ⁸	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
A	EP, A, 0110702 (ATLANTIC RICHFIELD) 13 June 1984	1-80
A	FR, A, 2506294 (SHELL FRANCAISE) 26 November 1982	1-80
A	US, A, 4472267 (YOO et al.) 18 September 1984 cited in the application	1-80
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IV. CERTIFICATION		
Date of the Actual Completion of the International Search		Date of Mailing of this International Search Report
13th July 1987		31 JUL 1987
International Searching Authority		Signature of Authorized Officer
EUROPEAN PATENT OFFICE		M. VAN MOL 

ANNEX TO THE INTERNATIONAL SEARCH REPORT ON

INTERNATIONAL APPLICATION NO.

PCT/US 87/00749 (SA 16866)

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Patent document cited in search report	Publication date	Patent family member(s)	Publication date
EP-A- 0110702	13/06/84	AU-A- 1895283	07/06/84
		JP-A- 59131568	28/07/84
		US-A- 4522937	11/06/85
		CA-A- 1201699	11/03/86
FR-A- 2506294	26/11/82	None	
US-A- 4472267	18/09/84	EP-A- 0045170	03/02/82
		AU-A- 7189981	04/02/82
		CA-A- 1162522	21/02/84
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		JP-A- 58047087	18/03/83
		AU-A- 7956882	24/03/83
		US-A- 4495305	22/01/85
		AU-B- 557769	08/01/87

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